CHE 4253

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Process Engineering Economics

2-Equipment Cost Estimation, Depreciation & Product Cost

Expressed as the cost of the equipment delivered to the site + the cost of installation. Sometimes comes separate.

Expressed as a function of equipment capacity.

	E= a CI ^b
Sometimes	E=c+ a CI ^b

CI: equipment capacity indicator (Areas, diameters, number of trays, power)

a: Cost coefficient b: Scaling c: Fixed cost



Expressed as a function of equipment capacity





PIPING:





PUMPS:



Centrifugal



Reciprocating



REACTORS:





HEAT EXCHANGERS





COLUMNS





Exponent b in $E = a Ci^{b}$

Equipment	Size range	Exponen
Blender, double cone rotary, carbon steel (c.s.)	1.4-7.1 m ³ (50-250 ft ³)	0.49
Blower, centrifugal	0.5-4.7 m ³ /s (10 ³ -10 ⁴ ft ³ /min)	0.59
Centrifuge, solid bowl, c.s.	7.5-75 kW (10-10 ² hp) drive	0.67
Crystallizer, vacuum batch, c.s.	15-200 m ³ (500-7000 ft ³)	0.37
Compressor, reciprocating, air-cooled, two-stage, 1035-kPa discharge	0.005-0.19 m ³ (10-400 ft ³ /min)	0.69
Compressor, rotary, single-stage, sliding vane, 1035-kPa discharge	0.05-0.5 m3/s (102-103 ft3/min)	0.79
Dryer, drum, single vacuum	$1-10 \text{ m}^2 (10-10^2 \text{ ft}^2)$	0.76
Dryer, drum, single atmospheric	$1-10 \text{ m}^2 (10-10^2 \text{ ft}^2)$	0.40
Evaporator (installed), horizontal tank	$10-1000 \text{ m}^2 (10^2-10^4 \text{ ft}^2)$	0.54
Fan, centrifugal	0.5-5 m ³ /s (10 ³ -10 ⁴ ft ³ /min)	0.44
Fan, centrifugal	10-35 m ³ /s (2×10 ⁴ -7×10 ⁴ ft ³ /min)	1.17
Heat exchanger, shell-and-tube, floating head, c.s.	10-40 m ² (100-400 ft ²)	0.60
Heat exchanger, shell-and-tube, fixed sheet, c.s.	10-40 m ² (100-400 ft ²)	0.44
Kettle, cast-iron, jacketed	1-3 m ³ (250-800 gal)	0.27
Kettle, glass-lined, jacketed	0.8-3 m ³ (200-800 gal)	0.31
Motor, squirrel cage, induction, 440-V, explosion-proof	4-15 kW (5-20 hp)	0.69
Motor, squirrel cage, induction, 440-V, explosion-proof	15-150 kW (20-200 hp)	0.99
Pump, reciprocating, horizontal cast-iron (includes motor)	1×10^{-4} -6×10 ⁻³ m ³ /s (2-100 gpm)	0.34
Pump, centrifugal, horizontal, cast steel (includes motor)	4-40 m ³ /s·kPa (10 ⁴ -10 ⁵ gpm·psi)	0.33
Reactor, glass-lined, jacketed (without drive)	0.2-2.2 m ³ (50-600 gal)	0.54
Reactor, stainless steel, 2070-kPa	0.4-4.0 m ³ (10 ² -10 ³ gal)	0.56
Separator, centrifugal, c.s.	1.5-7 m ³ (50-250 ft ³)	0.49
Tank, flat head, c.s.	0.4-40 m ³ (10 ² -10 ⁴ gal)	0.57
Tank, c.s., glass-lined	0.4-4.0 m ³ (10 ² -10 ³ gal)	0.49
Tower, c.s.	5×10^{2} -10 ⁶ kg (10 ³ -2×10 ⁶ lb)	0.62
Tray, bubble cap, c.s.	1-3 m (3-10 ft) diameter	1.20
Tray, sieve, c.s.	1-3 m (3-10 ft) diameter	0.86



DEPRECIATION

Reduction in value due to any causes.

Example: Pump

 Cost :
 $C_V = $12,000$

 Scrap value :
 $V_S = $2,000$

Depreciation: $C_V - V_S = $10,000$

For engineers, depreciation is considered as a cost for using the equipment.





Types Of Depreciation

<u>Physical</u>: Wear and Tear, corrosion, accidents, age deterioration.

Functional: All other causes.

<u>Obsolescence</u>: Due to technological advances.

<u>Depletion</u>: Loss due to materials consumed. Applicable to Natural Resources (timber, mineral, oil deposits)

IRS: "A reasonable allowance for the exhaustion, wear and tear of property used in the trade or business including a reasonable allowance for obsolescence"



DEPRECIATION

Methods To Calculate Depreciation

1. <u>Straight Line Depreciation</u>:

Value decreases linearly in time.

 $D = (V - V_S)/n$

D: Depreciation (\$/year) V : Original value V_S: Salvage value. n : Service life

<u>Book Value :</u>

$$V_a = V - a D$$

a : number of years of use.



2. <u>Multiple Straight Line Depreciation:</u>

Re-estimates the service life and salvage value at the end of every accounting period.

3. <u>Declining balance or Fixed % Method:</u>

Depreciation (D) is a fixed % of the property value at the beginning of the year.

Let f be the fixed % factor.

End of first year : $D_1 = V f$ $V_a = V - V f = V(1 - f), a = 1$ End of 2nd year : $D_2 = V(1 - f) f$ $V_a = V(1 - f)^2, a = 2$



3. <u>Declining balance or Fixed % Method:</u>

End of nth year : $D_n = V(1-f)^{n-1} f$ $V_a = V(1-f)^n = V_s$ ==> $f = 1 - \left(\frac{V_s}{V}\right)^{1/n}$ (Matheson Formula)

Emphasis on salvage value. Not used. What if $V_s=0$?



4. Double Declining Method:

Tax laws allow for depreciation up to twice the value calculated from the straight line method.

f=2/n

Consider n=10. Then f=2/10

After 5 years:

 $V_a = V(1-f)^5$

and $(V_a / V) = (1 - 0.2)^5 \sim 0.32$

Approximately 2/3 is written off after 1/2 life if n=10.



4. Double Declining Method:

Book value as a percentage at half life:

n	(1-2/n) ^{n/2}		
4	0.25		
6	0.29		
8	0.31		
10	0.32		
20	0.35		

5. <u>Combination Method</u>

The Combination Method assumes first half-life : Double declining Second half-life : Straight line



6. Modified Accelerated Cost Recovery System (MACRS):

It is essentially a combination method allowed by the IRS.

Uses double declining initially, and then switches to straight line.

When does the switch happen? When f for straight line is higher than f for double declining! (This is the IRS!)

Half year convention: In the first year only half of the double declining method depreciation is allowed. As a result, the process is depreciated half a year after its economic life!

(This is the IRS!) MACRS- Example (see Table 9.2, in TBW&S):





RECIPE

Raw materials Operating labor Operating supervision Utilities Electricity Fuel Refrigeration Steam Waste treatment and disposal Water, process Water, cooling Maintenance and repairs Operating supplies Laboratory charges Royalties (if not on lump-sum basis) Catalysts and solvents Depreciation Taxes (property) Financing (interest) Insurance Rent Medical Safety and protection General plant overhead Payroll overhead Packaging Restaurant Recreation Salvage Control laboratories Plant superintendence Storage facilities Executive salaries Clerical wages Engineering Legal costs Office maintenance Communications Sales offices Sales personnel expenses Shipping Advertising Technical sales service Research and development

Subtotal: Variable production costs

Subtotal: Fixed charges

Subtotal: Plant overhead costs Total of above = Manufacturing costs

Subtotal: Administrative expenses

Subtotal: Distribution and marketing expenses

Total of administrative, distribution and marketing, R&D = General expenses Total of all above = Total product cost

Careful with

- Utilities
- Depreciation
- Not all items apply



PRODUCT COST

RECIPE

Title:	Date:				
Product: Operating time, h/yr: Capacity, kg/yr:		Capacity, kg/ł Capacity, kg/s Fixed Capital User var	,		
	Suggested factor	Rate or quantity per year	Cost per rate or quantity unit	Calculate values, \$1	
Raw materials					
1					
2					
3					
4				Total	
Operating labor				xotati	
Operating supervision	0.15	of operating la	of operating labor		
Water					
Cooling					
Process					
Electricity					
Enel					
Potricerstion					
Reingeration					
Steam					
Waste treatment and dispos	a1			_	
Maintenance and repairs	0.07	of FCI			
Operating supplies	0.15	of maintenanc	e and repairs		
Laboratory charges	0.15	of operating la	bor		
Royalties (if not on lump-sum basis	s) 0.04	of TPC without	t depreciation		
Catalysts and solvents					
		Total va	riable productio	n costs	
Depreciation-calculated separate?	v below		producero	u costa	
Taxes (property)	0.02	of ECI			
Financing (interest)	0.00	of PCI			
Incurance	0.00	of PCI			
Dent	0.01	of PC1			
Kellt	0.00	of PC1			
			Fixed c	harges	
			(without depred	ciation)	
			Plant overhead costs.		
			Administrativ	e costs	
		I	Distribution + ma	rketing	
				costs	
		te	search and develo	oppent	
			General ex	penses	
			Total produ	ct cost	
			(without denner	istion)	
			(without deprec	siation)	

