

# **Development of an Arsenic Mitigation Strategy for Bangladesh**

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University of Oklahoma – May 4, 2006



# Introduction

- 80 million people in Bangladesh are exposed to toxic levels of arsenic in well water
- The goal of this project was to develop an arsenic mitigation plan by designing an arsenic removal device that provides potable water



# Introduction

- Four arsenic removal devices were considered:
  - **Activated Alumina** (designed)
  - Reverse Osmosis (designed)
  - Arsenic BioSand Filter (literature)
  - Iron Oxide Coated Sand (literature)



# Introduction

- The community-sized activated alumina device was selected
  - Minimizes Cost
  - Maximizes sustainability and ease-of-use
- Each device serves one well
  - Approximately 250 people
- The cost is \$4.79 per person, or \$383 million for countrywide implementation over ten years



# Arsenicosis

The various clinical manifestations caused by chronic arsenic toxicity due to prolonged drinking of arsenic-contaminated water, or chronic exposure to arsenic via other sources





# The Arsenic Problem

- Minor Health Effects
  - Hyper-pigmentation
    - Pigmentation alterations (hyper and hypo)
    - Melanosis
  - Hyper-keratosis
    - Thickening of the skin





# The Arsenic Problem

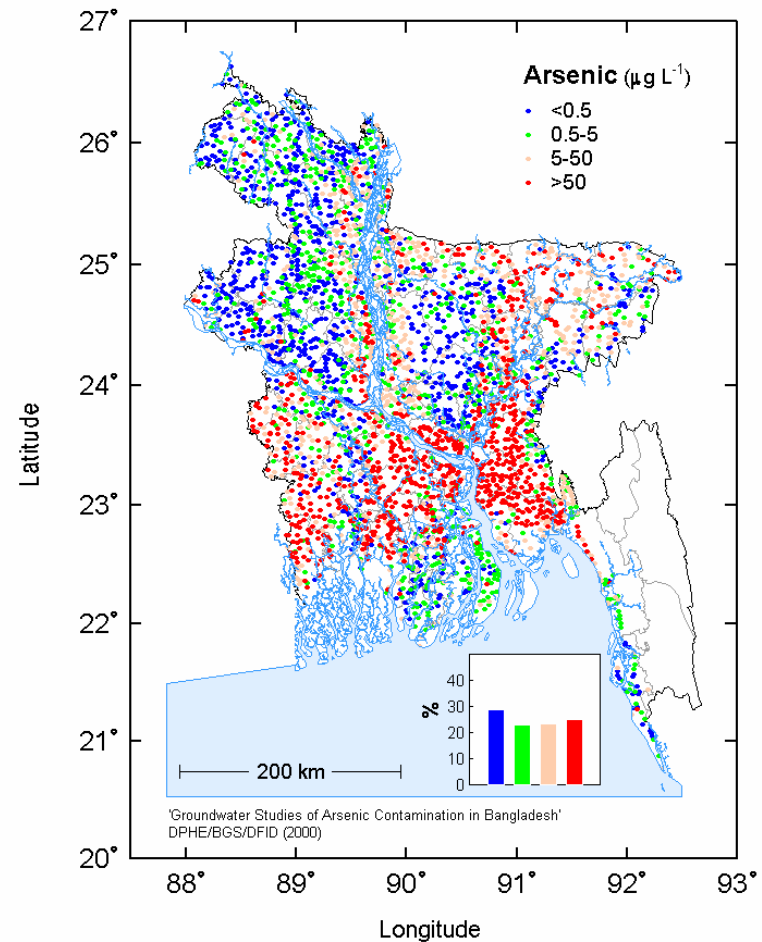
- Major Health Effects
  - Bronchitis
  - Liver Damage
  - External and Internal Malignancies
    - Extreme skin lesions





# The Arsenic Problem

- 30 Million at Extreme Risk
  - At risk of contamination levels  $> 50$  ppb
- 50 Million at High Risk
  - At risk of contamination levels  $> 10$  ppb





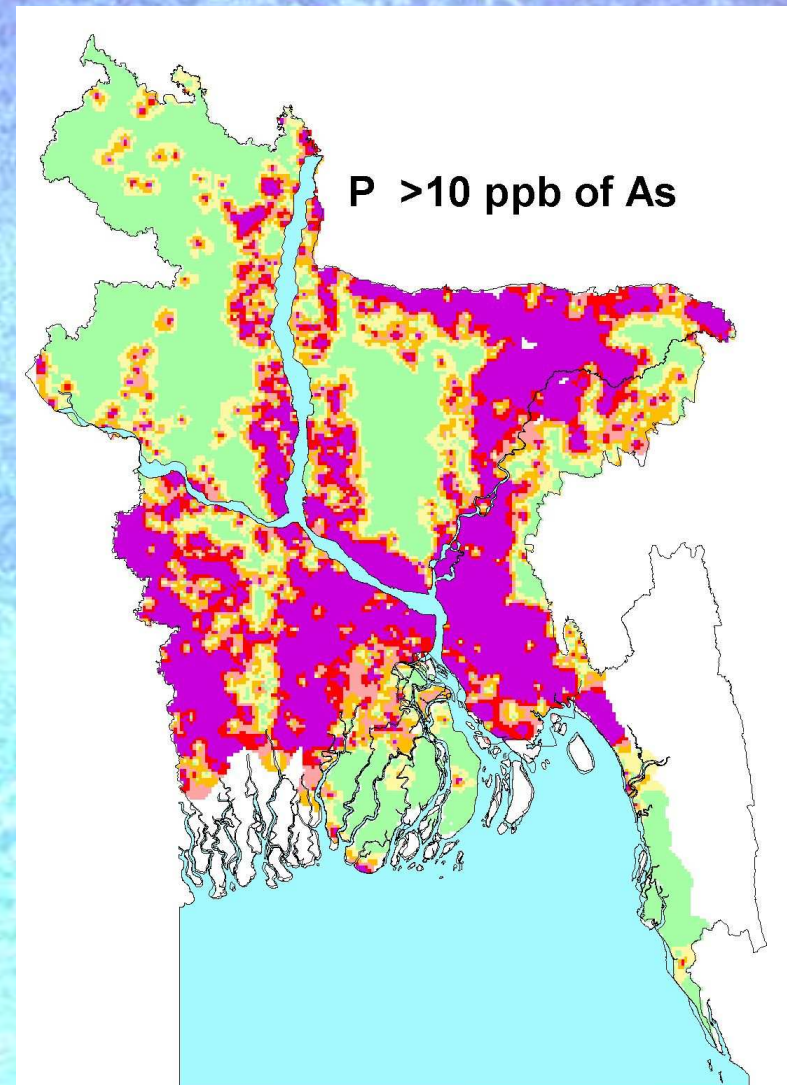
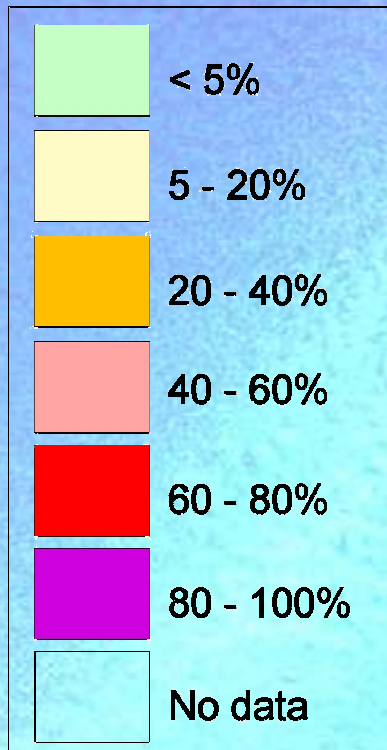
# The Arsenic Problem

- Over 100 million drink well water
- Piped water only serves 10% of the population.
- Surface to ground water switch started in 60's
- *Until arsenic discovery in 1993, well water was regarded safe for drinking*
- Geological origin of arsenic contamination



# The Arsenic Problem

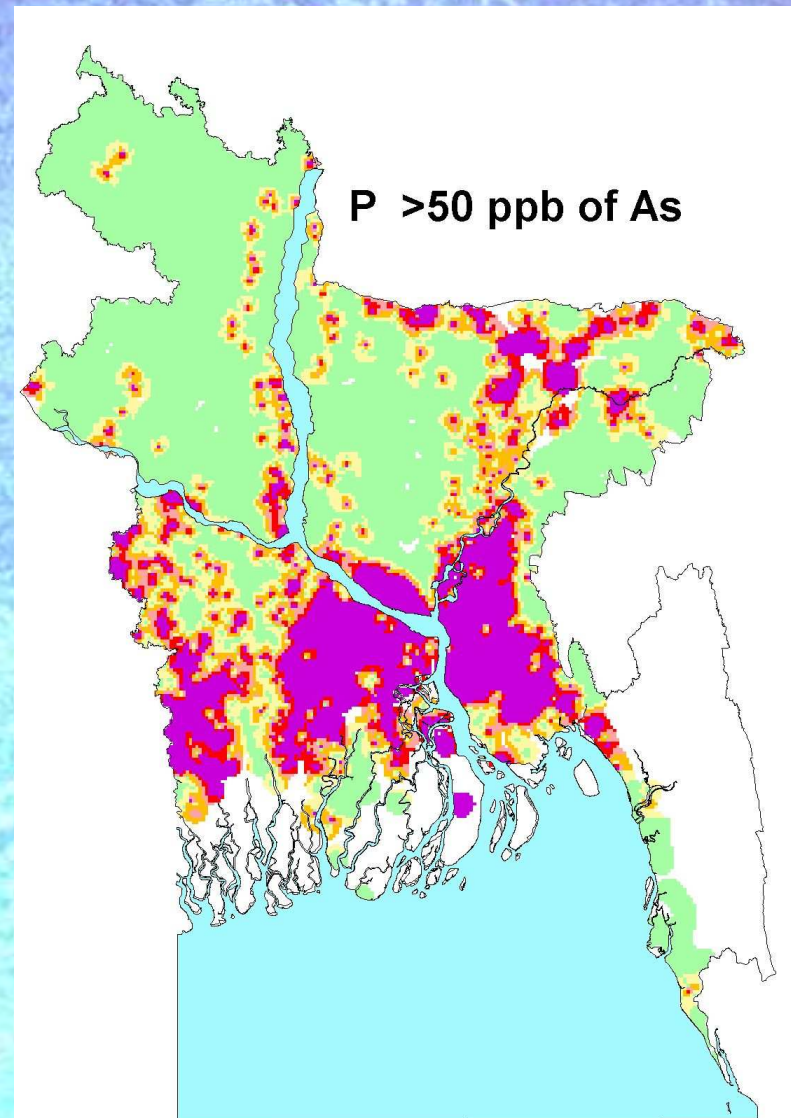
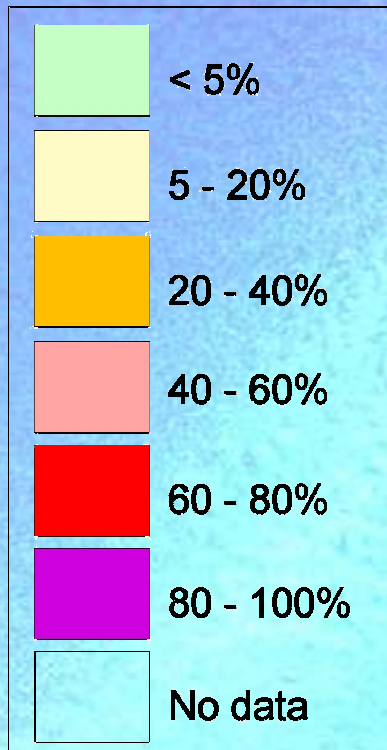
- Probability of locations exceeding various toxic thresholds





# The Arsenic Problem

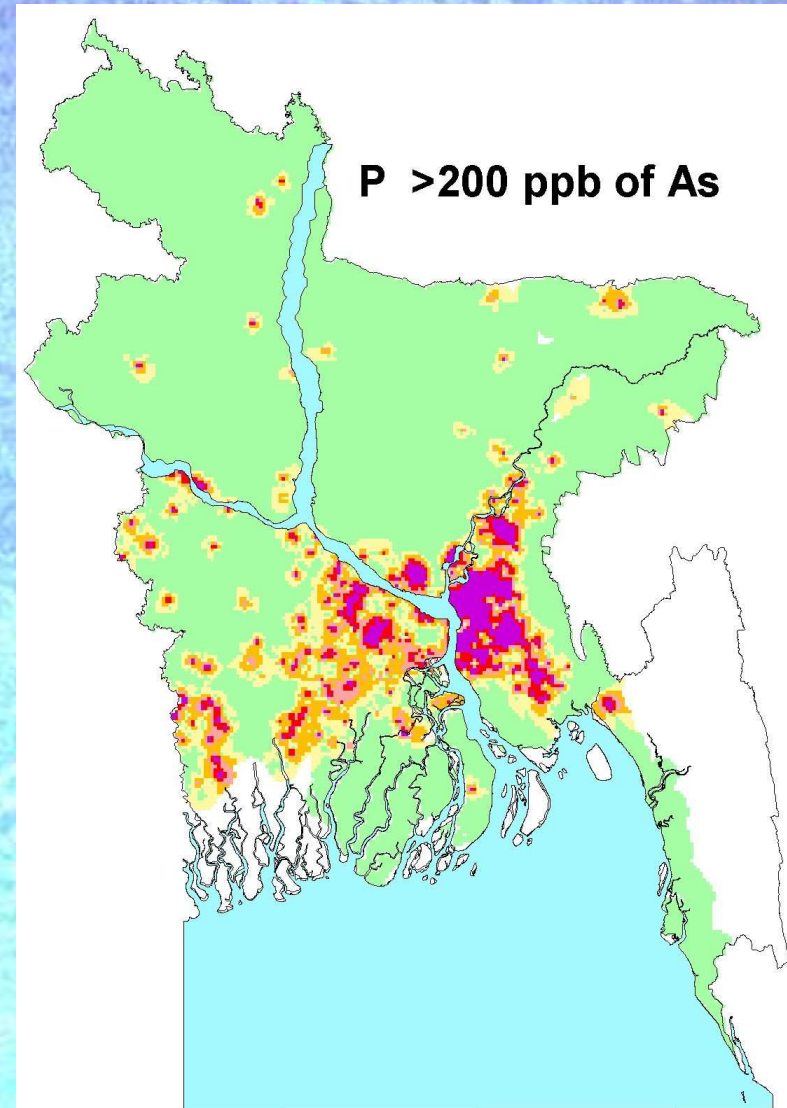
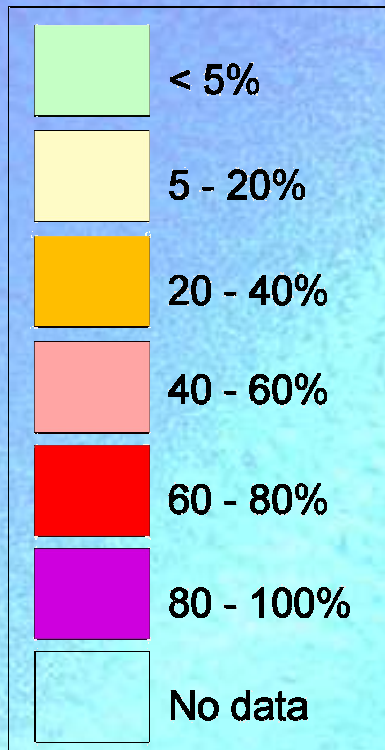
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# The Arsenic Problem

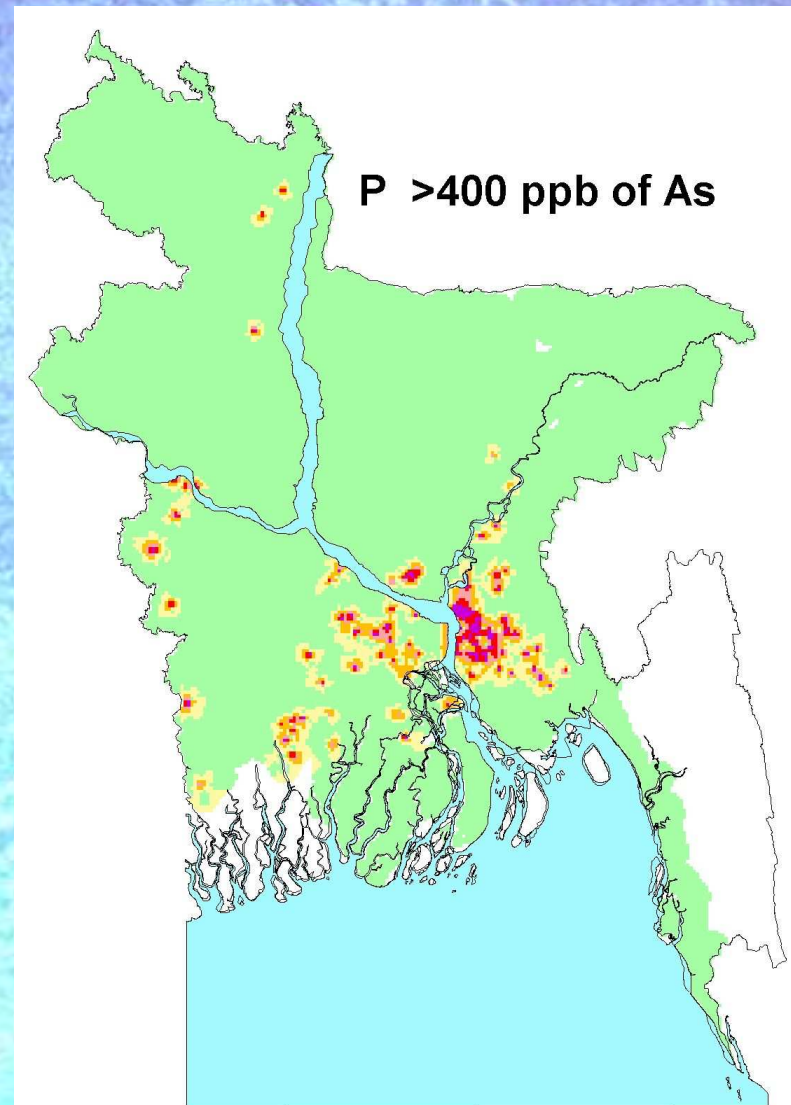
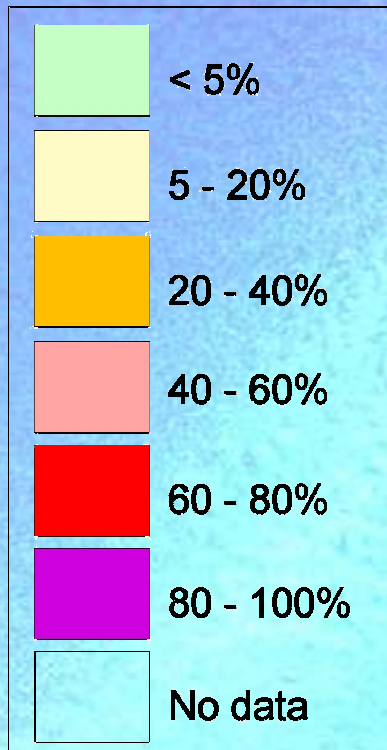
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# The Arsenic Problem

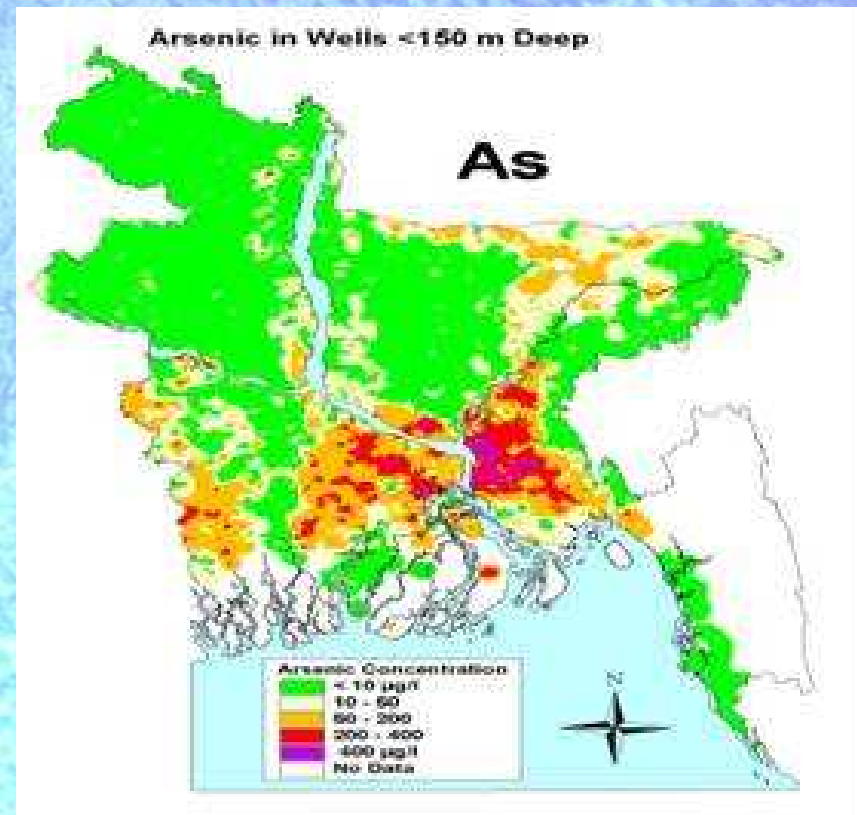
- Probability of locations exceeding various toxic thresholds





# Water Quality: Arsenic

<b>% of wells</b>	<b>Arsenic (ppb)</b>
37	10-50
15.9	50 – 200
7.3	200 – 500
1.7	500 – 1000
0.1	> 1000





# Water Quality

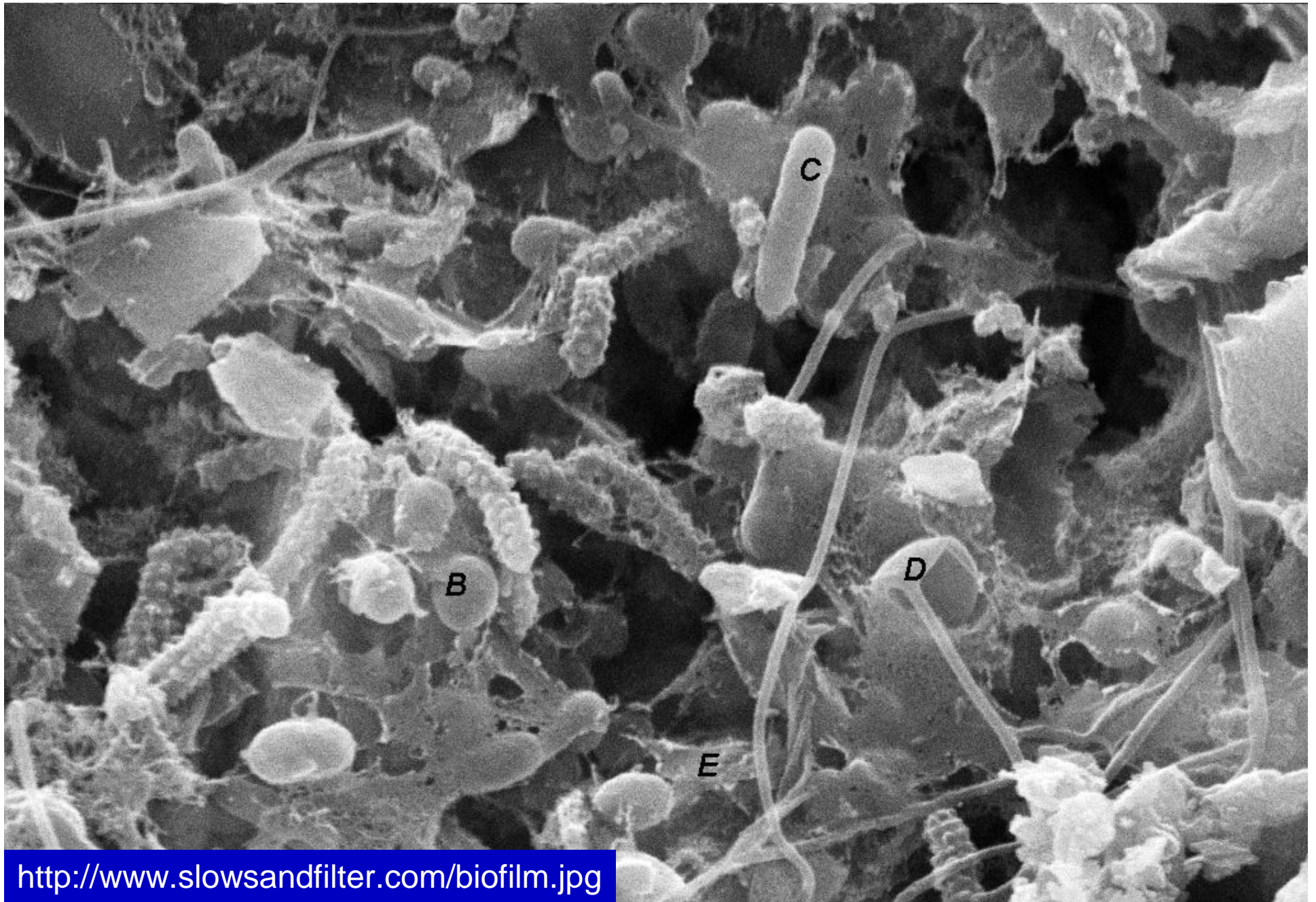
- Antimony, Cadmium, Chromium, Copper, Lead, Manganese, Molybdenum and Nickel levels all meet World Health Organization (WHO) standards
- 5% of wells have high boron levels
- High iron levels (1.1 mg/L)
  - No health risk, reduced by slow sand filter
- Low turbidity (few visible particles)



# Slow Sand Filtration

- Each of the designs considered uses slow sand filtration to pre-filter the water to remove pathogens and larger particles
- A bio-film layer on top of the sand accomplishes the removal
  - Consists of algae, bacteria, and protozoa
  - Takes several weeks to “ripen”





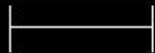
<http://www.slowsandfilter.com/biofilm.jpg>

EHT=25.00 kV

WD= 5 mm

Detector= SE1

1 $\mu$ m



The Robert Gordon University, Aberdeen

**FIGURE 3**



# Slow Sand Filtration

- Removal characteristics:
  - Turbidity (<1.0 NTU)
  - Pathogens (90-99%)
  - Heavy metals (Zn, Cu, Cd, Pb. 95-99%)
  - Arsenic (<47%)
  - Iron and manganese (>67%)



# Slow Sand Filter Design





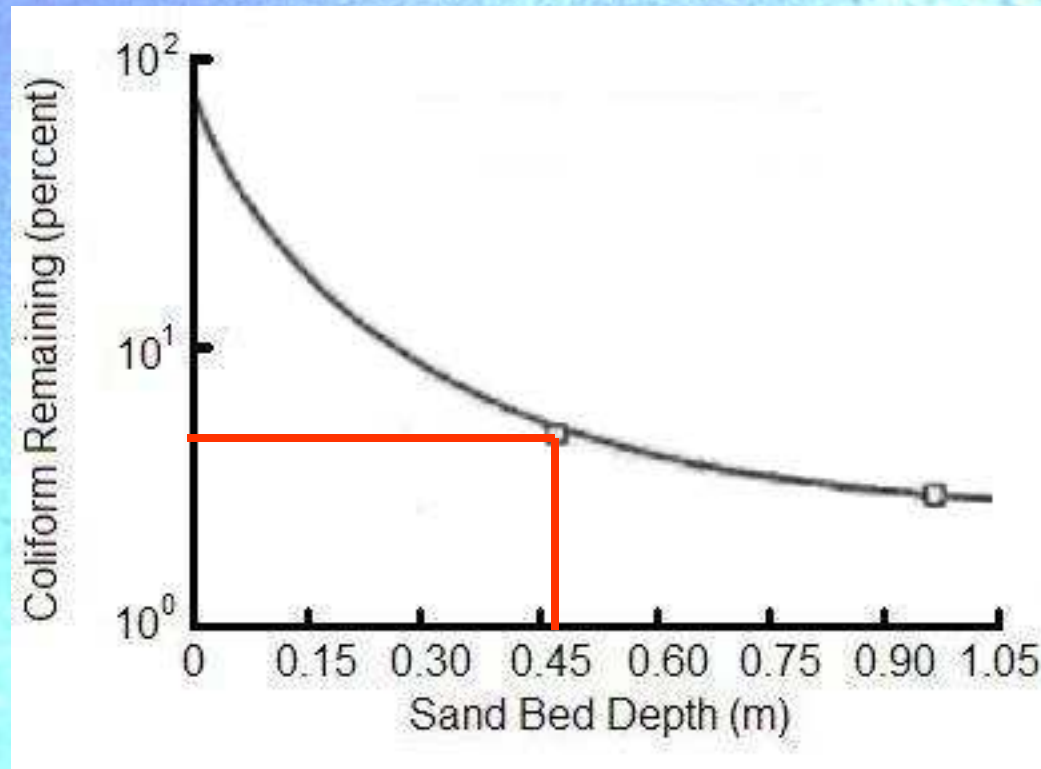
# Slow Sand Filter Design

Variable	Optimized Value
Sand size (diameter)	0.35 mm
Tank diameter	170 cm
Sand bed depth	50 cm
Supernatant Water Height	35 cm
Maximum hydraulic loading	400 L/hour
Maintenance type	Wet harrowing



# Slow Sand Filter Design

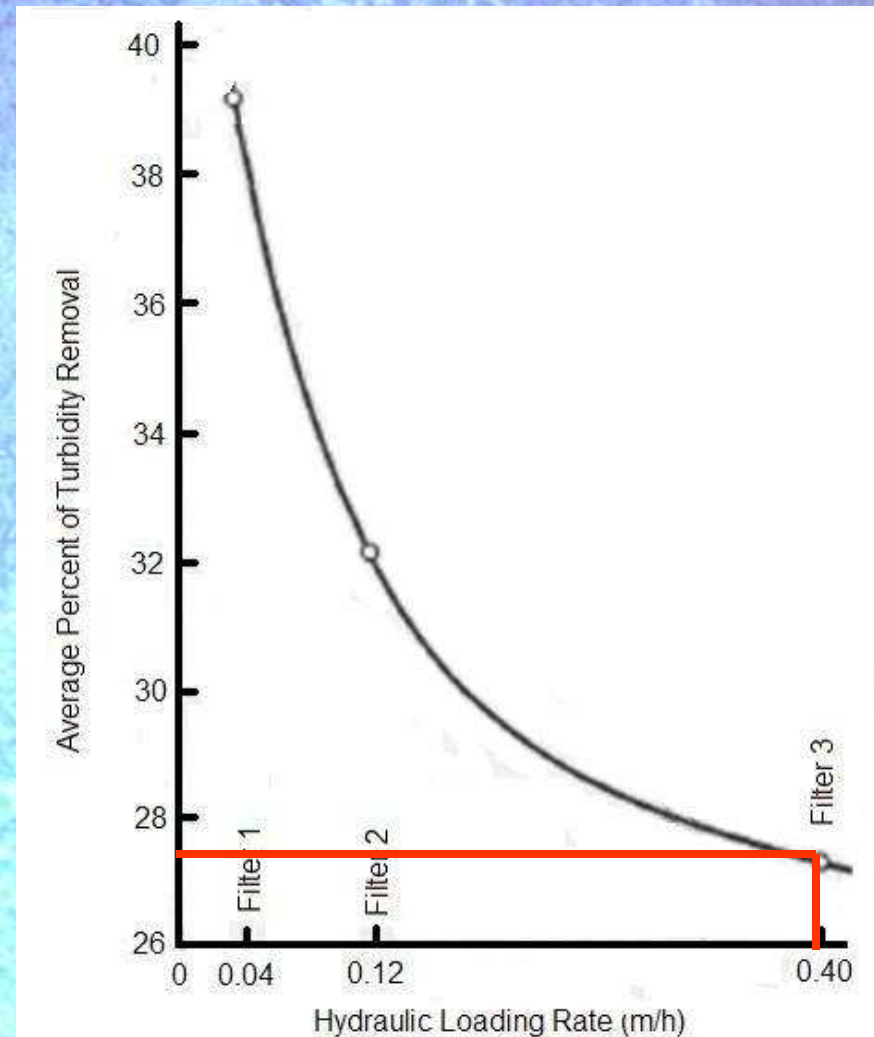
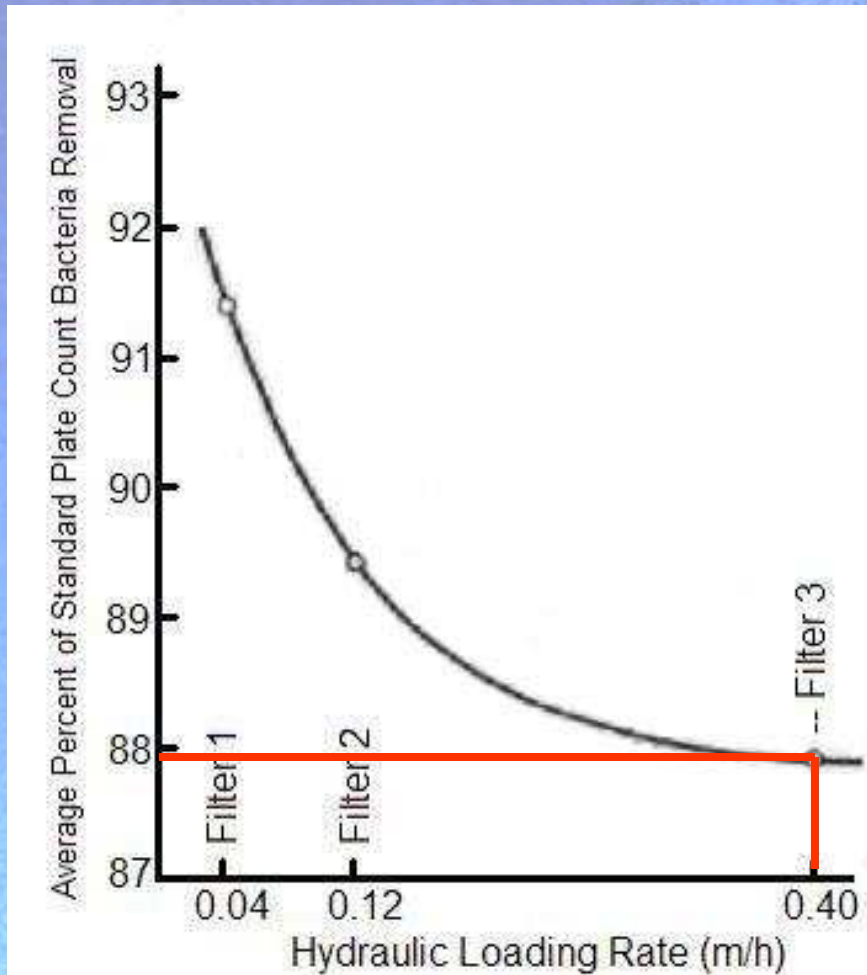
- Data from literature was used to determine the optimal sand filter properties



Bellamy, et. al. "Removing Giardia Cysts With Slow Sand Filtration."



# Slow Sand Filter Design



Bellamy, et. al. "Slow Sand Filtration: Influences of Selected Process Variables."

Bellamy, et. al. "Removing Giardia Cysts With Slow Sand Filtration."



# Slow Sand Filter Maintenance

- As the bio-film layer increases, the flow rate through the filter decreases
- Maintenance is required when the flow rate decreases to an unacceptable level
  - Estimated every 6 months from literature and water quality data



# Slow Sand Filter Maintenance

- Maintenance will be performed using the wet harrowing method
  1. The bio-film layer is agitated with a rake, suspending parts of the bio-film layer in the water
  2. The water is removed from the top
  3. Repeated until a significant amount of the bio-film is removed



# Slow Sand Filter Construction

- Begin with large container
  - 170 cm diameter
- Shop construction
  - Placement of hole near bottom
- On-site construction
  - Sand depth:
    - 1 meter fine sand
    - 10 cm gravel
  - Standing water depth: 35 cm
  - 2 Polyester cloths to separate each layer
  - PVC Pipe attached and cemented



# Removal Technologies

- Coagulation
  - Followed by microfiltration
  - Disadvantages:
    - User-addition of liquid coagulant
    - Stirring required, mixing times up to 60 minutes
- Ion Exchange
  - Effective for city-scale arsenic removal
  - Disadvantage: Expensive resins



# Removal Technologies

- Adsorption
  - Iron oxide used in two comparison cases:
    - Iron oxide coated sand
    - Arsenic BioSand Filter (rusted nails)
  - Activated alumina
    - Selected for study
- Membrane Removal
  - Reverse osmosis selected for study



# Reverse Osmosis Theory

$$f_{1(\text{fresh})}^{\text{salty}} = f_1^{\text{fresh}}$$

$$\alpha_{\text{water}}^{(\text{salty})} f_{\text{water}}^{\circ} \{T, P_{\text{salty}}\} = \alpha_{\text{water}}^{(\text{fresh})} f_{\text{water}}^{\circ} \{T, P_{\text{fresh}}\}$$

$$\alpha_{\text{water}}^{(\text{salty})} = x_{\text{water}}^{(\text{salty})} \gamma_{\text{water}}^{(\text{salty})} \quad \alpha_{\text{water}}^{(\text{fresh})} = 1$$

$$x_{\text{water}}^{(\text{salty})} \gamma_{\text{water}}^{(\text{salty})} f_{\text{water}}^{\circ} \{T, P_{\text{salty}}\} = f_{\text{water}}^{\circ} \{T, P_{\text{fresh}}\}$$

If  $x_{\text{water}}^{\text{salty}} \gamma_{\text{water}}^{\text{salty}} < 1$ , then  $P_{\text{salty}} > P_{\text{fresh}}$

using the Poynting correction

$$f_{\text{water}}^{\circ} \{T, P_{\text{fresh}}\} = f_{\text{water}}^{\circ} \{T, P_{\text{salty}}\} \exp \left[ \frac{v_1 (P_{\text{salty}} - P_{\text{fresh}})}{RT} \right]$$

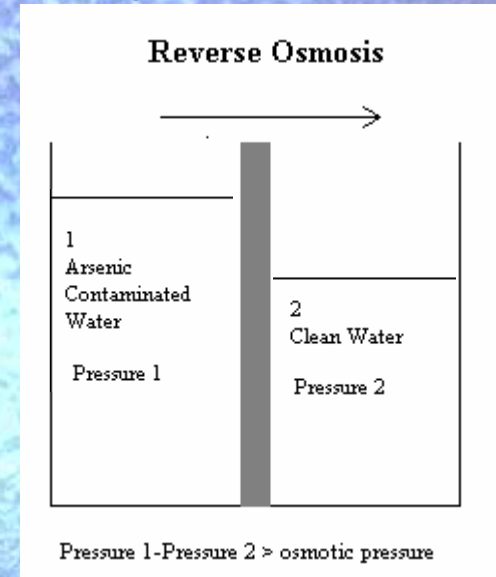
$$x_{\text{water}}^{\text{salty}} \gamma_{\text{water}}^{\text{salty}} f_{\text{water}}^{\circ} \{T, P_{\text{salty}}\} = f_{\text{water}}^{\circ} \{T, P_{\text{salty}}\} \exp \left[ \frac{v_1 (P_{\text{salty}} - P_{\text{fresh}})}{RT} \right]$$

Solving for  $P_{\text{salty}} - P_{\text{fresh}}$ , known as  $\pi$

$$\pi = (P_{\beta} - P_{\alpha}) = -\frac{RT}{v_1} \ln(x_1^{\beta} \gamma_1^{\beta})$$

Reduces to

$$\pi = -\frac{RT}{v_1} (-x_2^{\beta}) = RTc_2$$

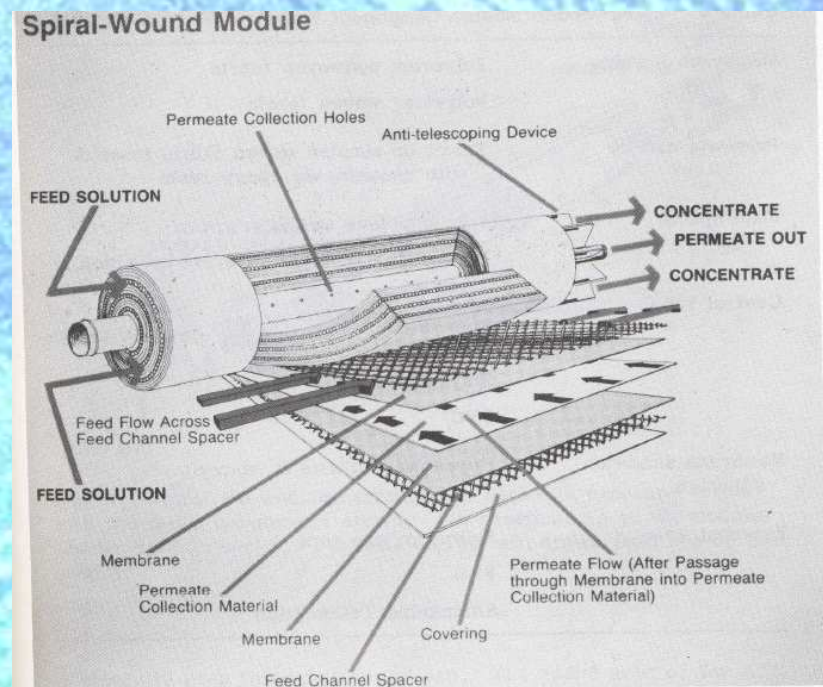




# Reverse Osmosis Theory

$$J_w = \frac{\text{mass permeation rate}}{\text{membrane area}} \quad (2\text{-}200 \text{ gal/ft}^2\text{/day or "gfd")}$$

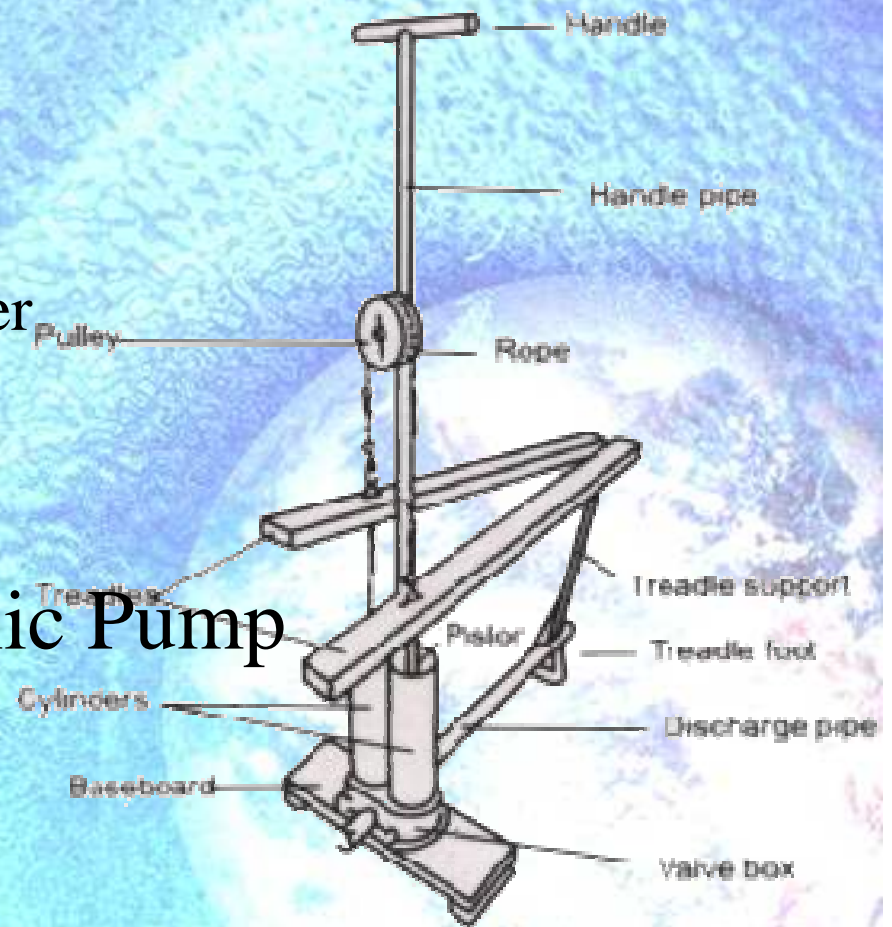
- Rejection Rate
  - 3 gal rejected per one gal treated  
(<http://wqa.org/>)
- Types
  - *Spiral-wound*
  - Plate-and-frame
  - Tubular
  - Hollow-fiber modules
- Brine – *critical issue*





# Reverse Osmosis

- Small Scale
  - Single home system most feasible due to pressure limitations
- Pre-Filter
  - Necessary pre-requisite
    - Satisfied by slow sand filter
- Hydraulics
  - The treadle pump
- Model MK1930 Hydraulic Pump
  - Used for cost estimation





# Reverse Osmosis

- RO System
  - Initial Installation – USRO 4-50 (50 gal/day)
  - \$133

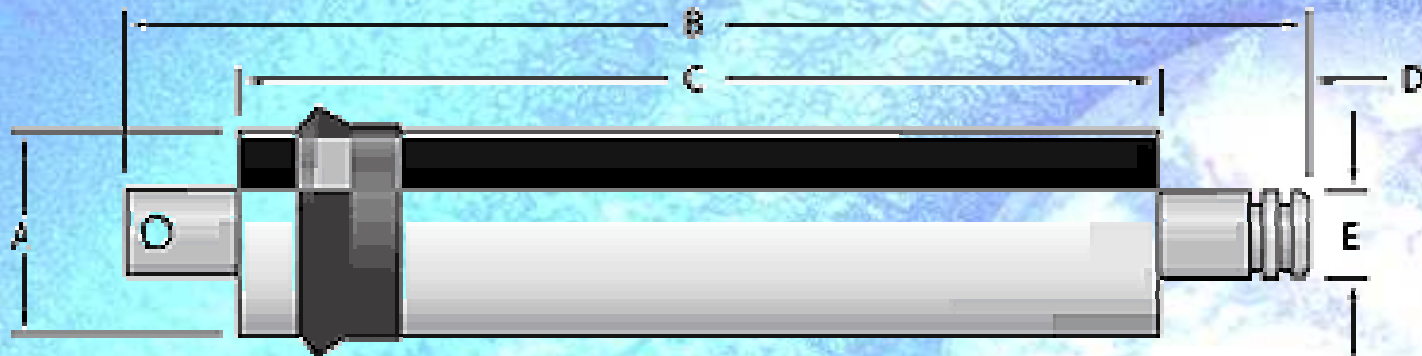
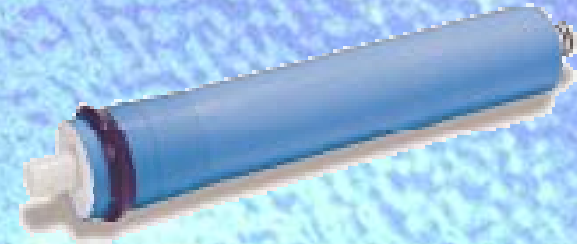


<http://www.h2ofilter.net/cat.asp?i=75>



# Reverse Osmosis

- Membrane Replacement
  - TM-50
  - Life Span – 3 year



<b>A: 1.80"</b>	<b>B: 11.75"</b>	<b>C: 10.00"</b>	<b>D: 0.875"</b>	<b>E: 0.678"</b>
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<http://www.h2ofilter.net/product.asp?i=464>



# Reverse Osmosis Material Cost

	Cost	Specs
RO System	\$133.00	
Storage Tank	\$3.00	
Bucket	\$3.00	Simple plastic
Pipe	\$2.50	
Sand	\$0.10	
Pump	\$150.00	High Pressure Hand
Total	\$290.00	

***Total Initial Instillation w/ RO – \$290***



# Reverse Osmosis Maintenance Cost

	Cost	Life Span	Yearly
Membrane	\$ 39.00	3	\$13.00
Storage Tank	\$ 3.00	2	\$1.50
Bucket	\$ 3.00	3	\$1.00
Pipe	\$ 2.50	6	\$0.42
Sand	\$ 0.10	6	\$0.02
Pump	\$ 150.00	10	\$15.00

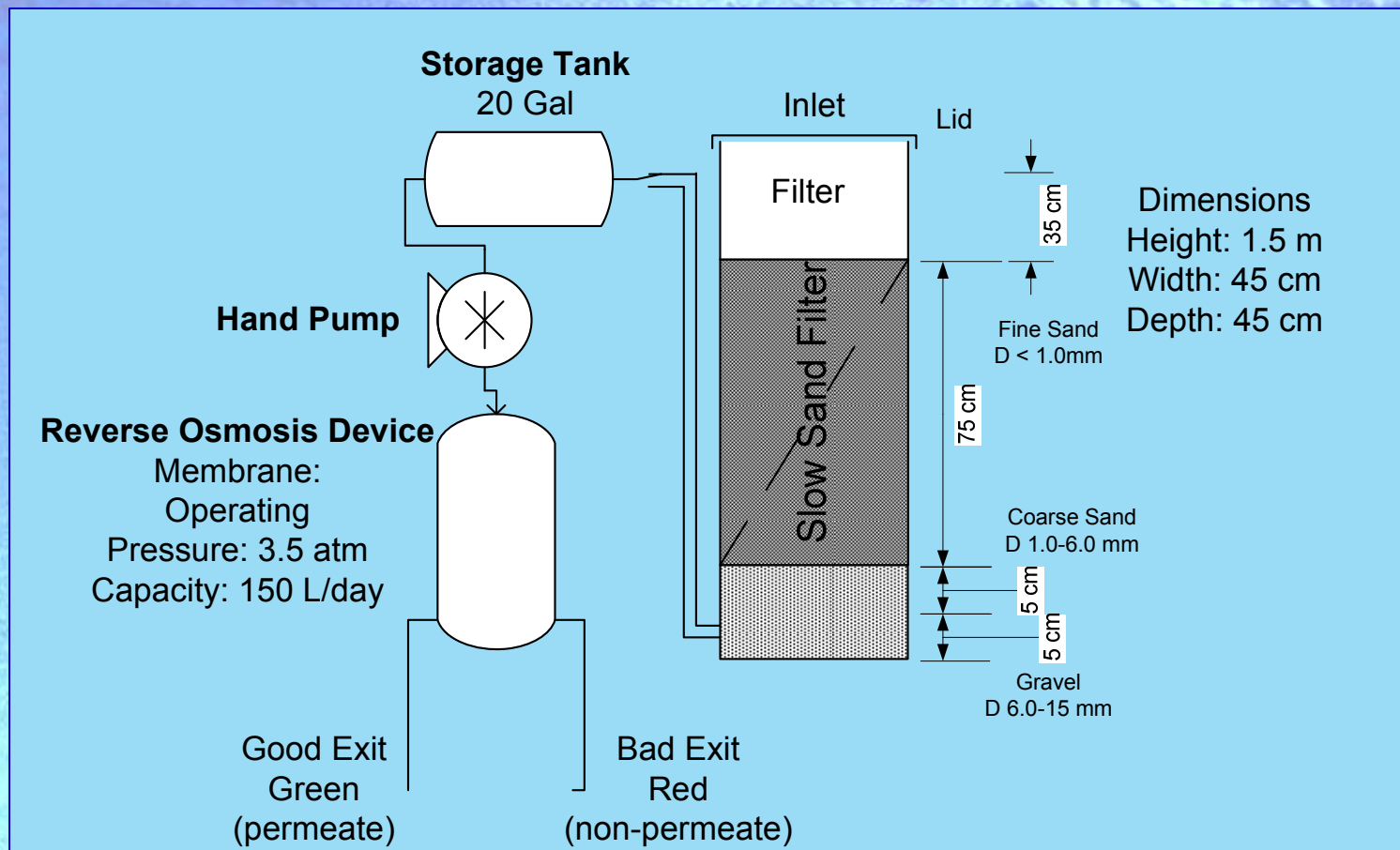
*Total Yearly for RO*

**\$32**



# RO PED

- Note: Two exit streams, one colored red, the other green





# RO Manufacturing

- Identical to slow sand filtration manufacturing
- Only modification is addition of RO system
  - Water is first collected in a storage tank
  - Passes through pump to enter RO device

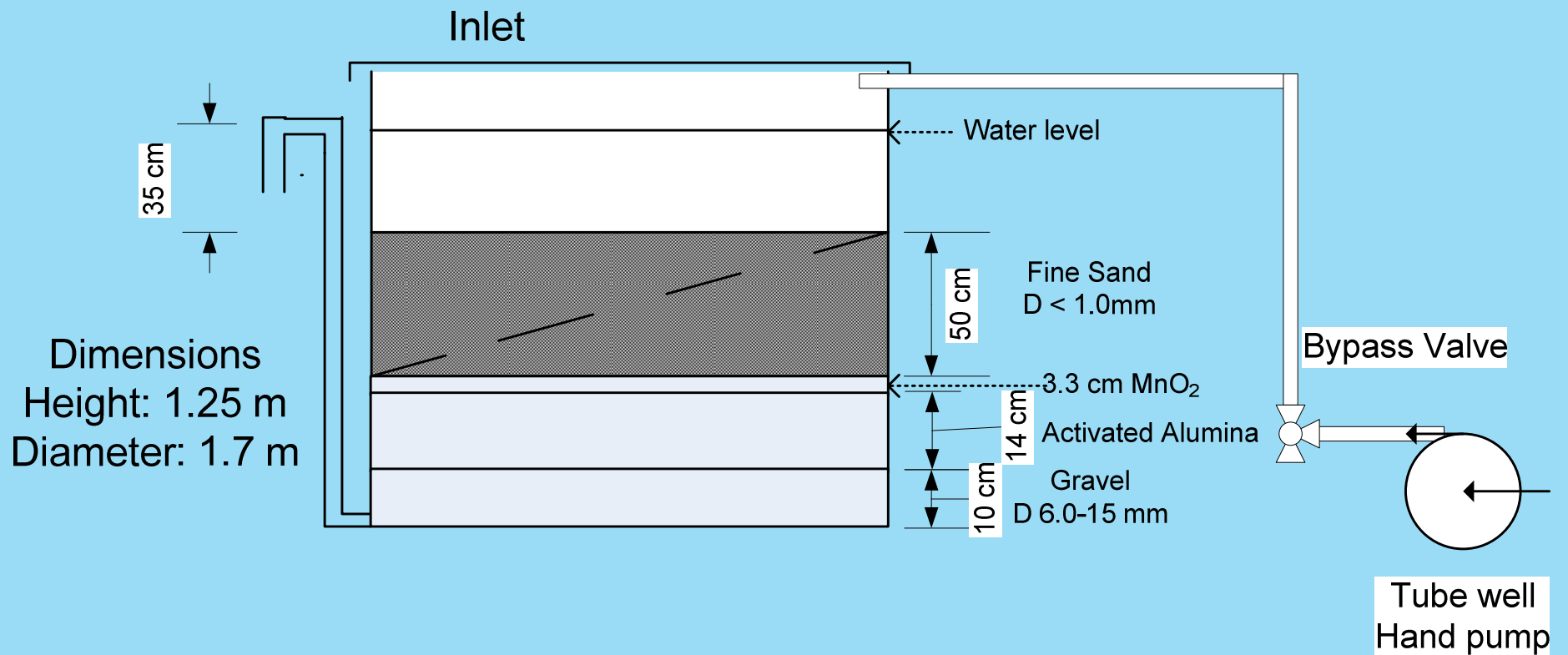


# Activated Alumina

- Process Flow Diagram
- Chemistry:
  - Oxidation from arsenite [As(III)] to arsenate [As(V)]
  - Adsorption onto activated alumina
- Design and Cost:
  - Determination of optimal unit lifetime from initial and maintenance costs



# Activated Alumina PFD





# Oxidation

- Activated alumina adsorbs arsenate much more strongly than arsenite
- Manganese dioxide\*
  - oxidizes 99.9% of arsenite to arsenate
  - empty bed contact time of 6 minutes
  - 1 ppm sulfur as a competing ion
  - Also adsorbs iron and manganese
    - ~67% of Fe and Mn are removed by sand

\*Ghurye and Clifford. "As(III) Oxidation using chemical and solid-phase oxidants." American Water Works Association. Jan 2004, 96



# Activated Alumina Chemistry

- Adsorption Selectivity
  - $\text{OH}^- > \text{H}_2\text{AsO}_4^- > \text{Si}(\text{OH})_3\text{O}^- > \text{HSeO}_3^-$   
>  $\text{F}^- > \text{SO}_4^{2-} > \text{CrO}_4^{2-}$   
>>  $\text{HCO}_3^- > \text{Cl}^- > \text{NO}_3^- > \text{Br}^- > \text{I}^-$
- Important competing ions:\*
  - Sulfate at 1.0 mg/L
  - Fluoride at 0.2 mg/L



<http://www.air-techengr.com>

\*Kinniburgh and Smedley, eds. "Arsenic Contamination of Groundwater in Bangladesh." *British Geological Survey Technical Report WC/00/19*, Volume 1



# Activated Alumina Design

<b>Physical Property</b>	<b>Size</b>
Diameter (cm)	170
Standing Water Height (cm)	35
Fine Sand Depth (cm)	50
Gravel Depth (cm)	10
MnO <sub>2</sub> Depth (cm)	3.3
Activated Alumina Depth (cm)	14
Total Unit Height (cm)	112.3
Total Unit Height (ft)	3.7
Mass of MnO <sub>2</sub> (kg)	114
Mass of Activated Alumina (kg)	254



# Activated Alumina Design

- Device cross-sectional area
  - Slow sand max hydraulic loading rate
  - Typical hand pump flow rate

$$A = \frac{\frac{15L}{\text{min}} * \frac{60 \text{ min}}{\text{hr}}}{400 \frac{L}{\text{m}^2 \text{ hr}}} = 2.25 \text{m}^2$$

- Corresponds to a 1.7 m diameter



# AA: Manganese Dioxide Layer

- The thickness of the manganese dioxide layer was determined by considering the empty-bed contact time requirement of six minutes

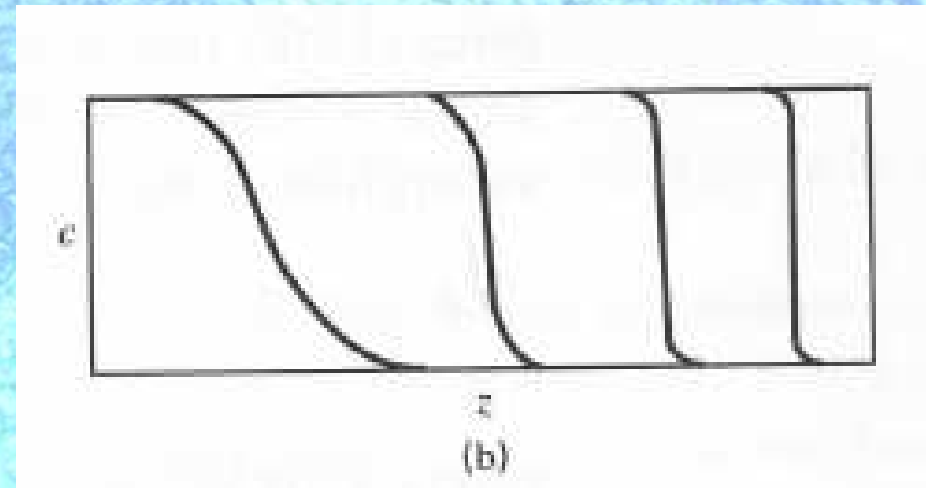
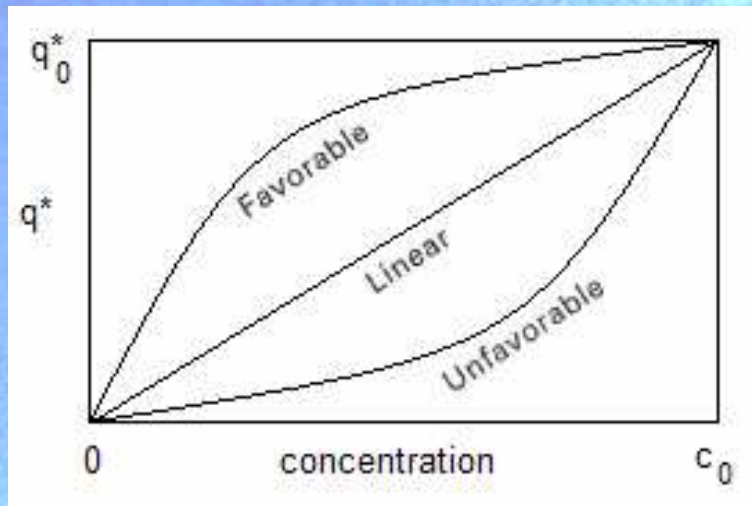
$$\text{EBCT} = \frac{\text{Height} * (\text{Cross - sectional Area})}{\text{Volumetric flow rate}}$$

- 3.3 centimeters



# Activated Alumina Design

- Arsenate has a favorable adsorption isotherm for activated alumina, leading to a self-sharpening adsorption wavefront



Seader, J.D. *Separation Process Principles*.  
(Hoboken: John Wiley & Sons, Inc., 1998). p.835



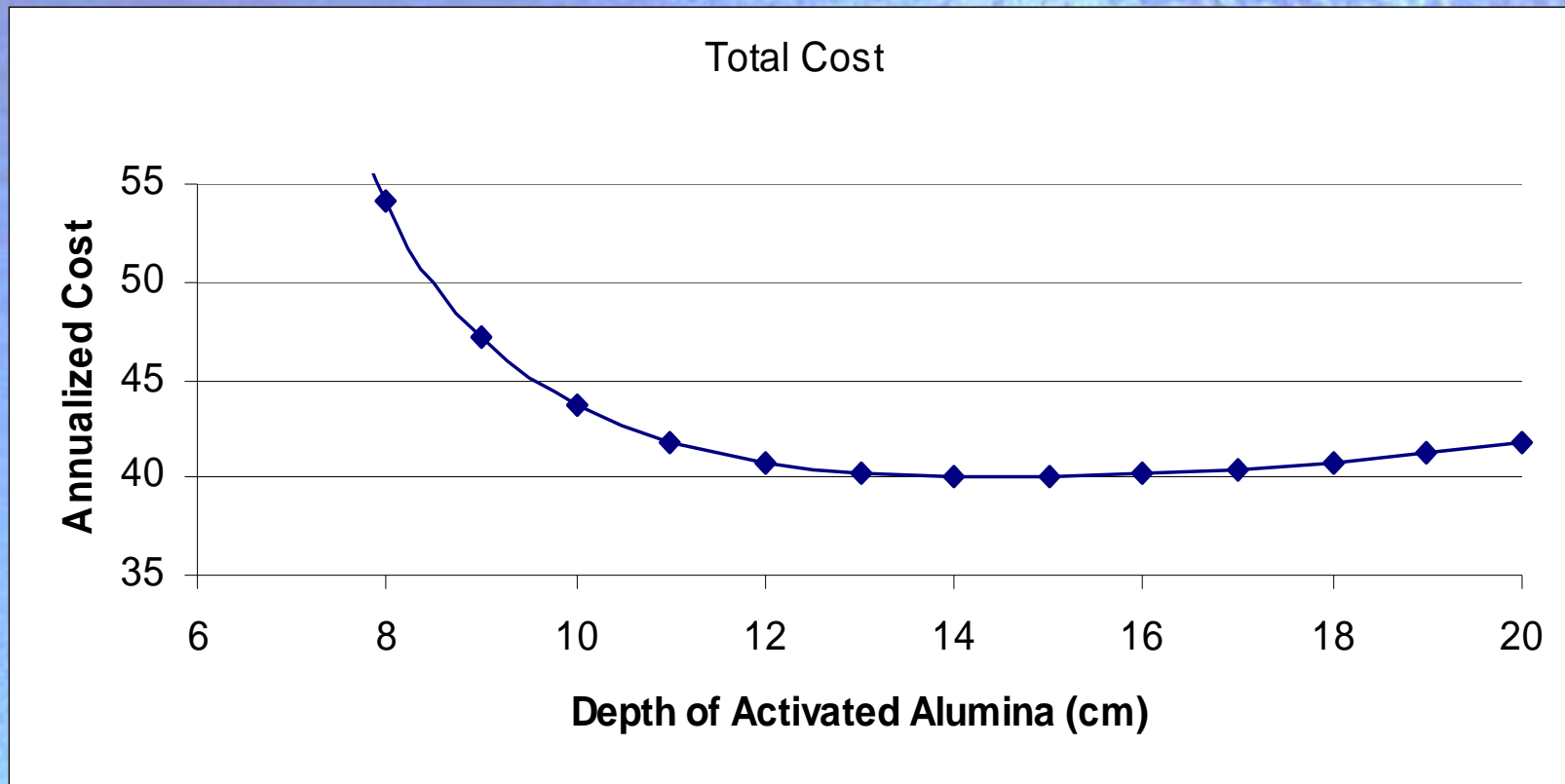
# Activated Alumina Design

- The required contact time for activated alumina is 12 minutes.\*
  - Minimum thickness: 6.6 cm
  - Optimal thickness: 14 cm (21 min contact time)
- An annual cost was determined by using straight line depreciation for the activated alumina, and adding the annual maintenance cost for each thickness.

\*Wang, et. al. "Arsenic Removal from Drinking Water by Ion Exchange and Activated Alumina Plants."



# Activated Alumina Design



\*Wang, et. al. "Arsenic Removal from Drinking Water by Ion Exchange and Activated Alumina Plants."



# Activated Alumina: Regeneration

- At pH's above 9.2, the surface of activated alumina becomes negative
- The negative surface repels the negatively charged arsenate ions
- A strong basic solution, such as potassium hydroxide or sodium hydroxide, can be used to regenerate the activated alumina



# Activated Alumina: Regeneration

- During regeneration, studies show that approximately 5% of the activated alumina becomes deactivated
- Probable causes:
  - OH<sup>-</sup> molecules adsorb as the basic solution is purged with well water and the pH drops below 9.2
  - Minor contributions from fouling or physical degradation of the alumina beads



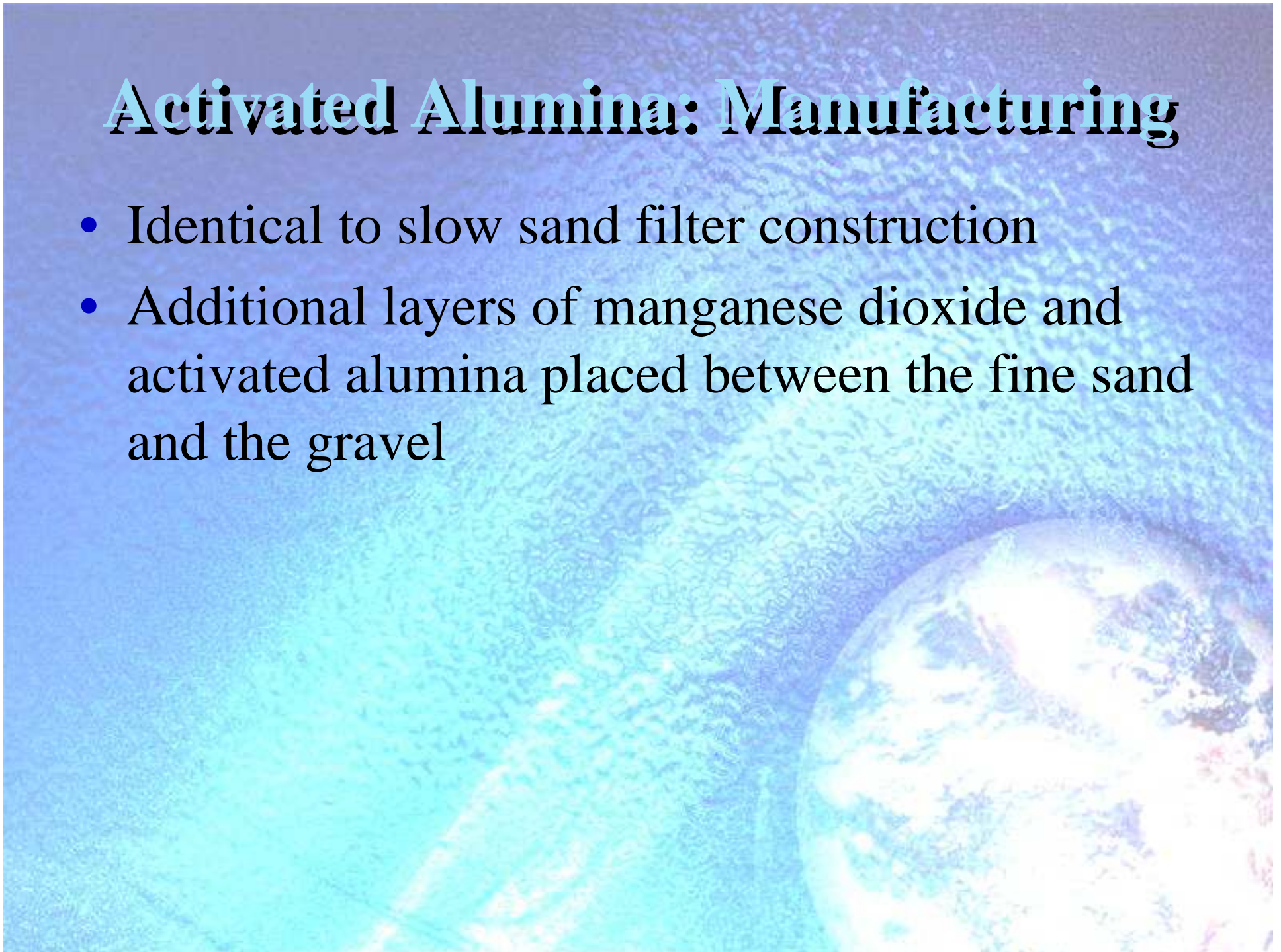
# Activated Alumina: Costs

Manufacturing Costs	
AA (\$3.125 / kg)	\$793.75
MnO <sub>2</sub> (\$0.525/kg)	\$59.85
Sand	\$1.77
Tank	\$250.00
Polyester Cloth	\$5.00
Labor	\$10.00
Piping	\$20.00
<b>Total</b>	<b>\$1,140.37</b>



# Activated Alumina: Manufacturing

- Identical to slow sand filter construction
- Additional layers of manganese dioxide and activated alumina placed between the fine sand and the gravel





# Comparison

## Advantages

AA – Cheap, Simple

RO – Simple Operation

IOCS – One Step Process

ABF – User Friendly

## Disadvantages

AA – Large OD- 5.6 ft

RO – Rejected water; Requires pressure

IOCS – IOCS; Manufacturing is complicated

ABF – Unconventional; Unproven



# Comparison

<u>Cost</u>	<u>Install</u>	<u>Maintenance</u>
AA	\$1140	\$29.33
RO	\$290	\$31
IOCS	N/A	N/A
ABF	\$40	N/A

<u>Cost/Person/Yr</u>	<u>Install</u>	<u>Maintenance</u>
AA	\$4.79	\$0.12
RO	\$29	\$3.10
IOCS	N/A	N/A
ABF	\$4.00	N/A



# Comparison

## Arsenic Removal

AA – Sufficient

RO – Sufficient

IOCS – Sufficient

ABF – Sufficient

## Design

AA – 2 Additional Steps: Oxidation & AA

RO – Additional RO system

IOCS – Substitute IOCS for fine sand

ABF – Additional Layer of Nails



# Comparison

## Lifetime

AA – 20 years for AA & MnO<sub>2</sub>

RO – replacement 3 years membrane replacement

IOCS – Replace/regenerate

ABF – N/A

## Maintenance

AA – Regenerate AA yearly

RO – Membrane lasts 3 years

IOCS – Must Replace Sand

ABF – Must Replace Nails



# Comparison

## Manufacture

AA – Very similar to slow sand

RO – Addition of RO unit

IOCS – Complicated IOCS manufacture

ABF – Addition of nail container

## Credibility

AA – Technically sound

RO – Trusted – Manufacturer

IOCS – OU Master Thesis Env. Engr.

ABF – MIT MBA Report

***WINNER IS...ACTIVATED ALUMINA!!***



# Pilot Testing

- Pilot testing will verify device performance, and identify areas of improvement in the design
- Recommended Location:
  - Gazipur Union (county-size area)
  - 1000 households
  - 300-500 ppb arsenic contamination
  - Low literacy



# Large-Scale Implementation

- Large-scale implementation
  - **Stage 1:** mitigate arsenic levels over 50 ppb
    - 30 million people at risk
    - Cost: \$150 million
  - **Stage 2:** mitigate arsenic levels between 10-50 ppb
    - 50 million people at risk
    - Cost: \$233 million



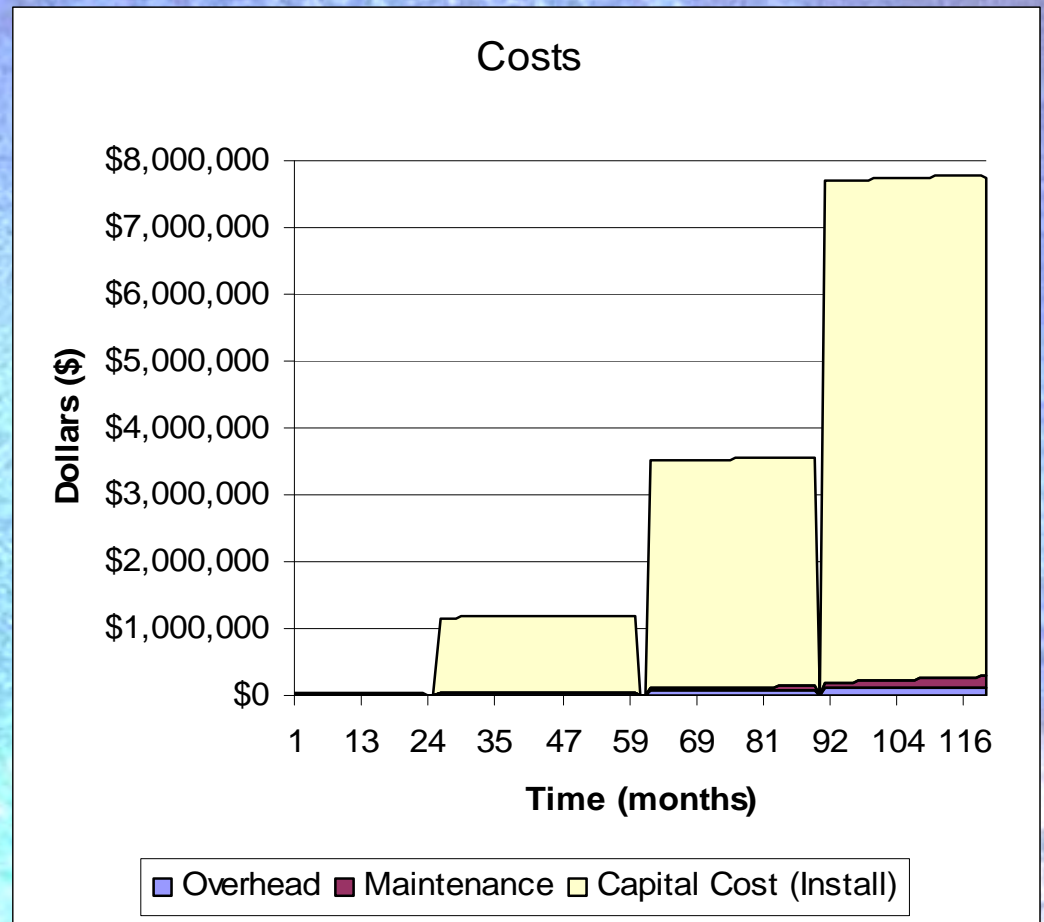
# Economic Plan

- Acquisition of Property
  - Rent for 1300 Sq. ft in Dhaka
    - \$270 per month ([www.velki.com/market](http://www.velki.com/market))
  - Cost of Business Startup in Dhaka, Bangladesh
    - \$370 - World Bank Economic Analysis
  - Labor
    - \$6 per unit in service per year



# Economic Plan

- Major component of costs is material costs





# Economic Plan

1-Jan-07	1-Jul-07	1-Jan-08	1-Jul-08	1-Jan-09	1-Jul-09	1-Jan-10	1-Jul-10	1-Jan-11	1-Jul-11	1-Jan-12	1-Jul-12	1-Jan-13	1-Jul-13	1-Jan-14	1-Jul-14	1-Jan-15	1-Jul-15	1-Jan-16	1-Jul-16	1-Jan-17
Stage One		Stage Two				Stage Three				Stage Four										
Phase One										Phase Two										

- Stage One
  - 20 units per month
- Stage Two
  - 1000 units per month
- Stage Three
  - 3000 units per month
- Stage Four
  - 6500 units per month



# Economic Plan - Funding

- Funding

- Government of Bangladesh - essential

- <http://www.bangladoot.org>

- World Bank



- Asian Development Bank (ADB)

- United Nations International Children's Fund (UNICEF)

- [http://www.unicef.org/bangladesh/wes\\_420.htm](http://www.unicef.org/bangladesh/wes_420.htm)

- United States Agency for International Development (USAID)



United States Fund for **unicef** 



# Conclusions

<b>Topic</b>	<b>Cost</b>	<b>Detail</b>
Initial Installation	\$1140	
Yrly. Maintenance (Including Main. Costs)	\$5.5	
Per Village	\$5,600	1000 People
Per District (Chandpur)	\$1,960,000	350,000 People
Phase 1 > 50 ppb (over 12 year plan)	\$150 million	To mitigate for 30 million people
Phase 2 > 10 ppb (over 10 year plan)	\$233 million	To mitigate for 50 million people



**Any Questions**

